

AMENDMENTS TO THE CLAIMS

Please amend the claims as follows:

1. (Currently Amended) A process for the preparation of a gas containing hydrogen and carbon monoxide from a carbonaceous feedstock and its conversion to a hydrocarbons containing stream, the process comprising:
 - (a) partially oxidizing a carbonaceous feedstock in a vertically oriented tubular partial oxidation reactor vessel having an upper end and a lower end, the vessel comprising a burner at the upper end, thereby obtaining an effluent comprising a first gaseous mixture of hydrogen and carbon monoxide;
 - (b) catalytically steam reforming a carbonaceous feedstock by feeding a feed of steam and the carbonaceous feedstock to a convective steam reformer comprising a tubular reactor provided with one or more tubes containing the reforming catalyst, wherein the steam to carbon molar ratio of the feed is below 1, to obtain a steam reforming product;
 - (c) feeding the steam reformer product to the upper end of the partial oxidation reactor to obtain a mixture of the effluent of step (a) and the steam reformer product; and
 - (d) providing heat for the steam reforming reaction in step (b) by convective heat exchange between the mixture obtained in step (c) and the steam reformer reactor tubes thereby obtaining a hydrogen and carbon monoxide containing gas having a reduced temperature;
 - (e) catalytically converting the hydrogen and carbon monoxide containing gas of step (d) using a Fischer-Tropsch catalyst into a hydrocarbons containing stream; and
 - (f) separating the hydrocarbons containing stream of step (e) into a hydrocarbon product comprising 5 or more carbon atoms and a gaseous recycle stream comprising nitrogen, unconverted methane and other feedstock hydrocarbons, unconverted carbon monoxide, carbon dioxide, hydrogen and water and recycling the recycle stream to step (a) and/or (b).
2. (Previously Presented) The process of claim 1, wherein the steam to carbon molar ratio of the feed to step (b) is between 0.5 and 0.9.
3. (Currently Amended) The process of claim 1, wherein the temperature of the mixture obtained in step (c) is between 800°C to 1050°C.

4. (Previously Presented) The process of of claim 1, further comprising autothermally reforming the mixture obtained in step (c).
5. (Previously Presented) The process of claim 2, wherein the temperature of the mixture obtained in step (c) is between 800°C to 1050°C.
6. (Previously Presented) The process of claim 2, further comprising autothermally reforming the mixture obtained in step (c).
7. (Previously Presented) The process of claim 3, further comprising autothermally reforming the mixture obtained in step (c).

Please add the following new claims.

8. (New) The process of claim 1, further comprising (g) hydrocracking/
hydroisomerizing the hydrocarbon product to form a middle distillate and a residue.
9. (New) The process of claim 8, further comprising subjecting the residue to catalytic dewaxing to obtain a base oil.
10. (New) The process of claim 8 further comprising feeding a portion of the steam reforming product to a hydrogen recovery unit to obtain hydrogen for use in step (g).